MENG366

System Types Error Constants

Dr. Saeed Asiri
saeed@asiri.net

Introduction

- ***Errors in a control system*** can be attributed to many factors:
  - **Imperfections in the system components** (*e.g.* static friction, amplifier drift, aging, deterioration, *etc*…)
  - **Changes in the reference inputs** $\rightarrow$ cause errors during transient periods & may cause steady-state errors.

- In this section, we shall investigate a **type of steady-state error that is caused by the incapability of a system to follow particular types of inputs**.

Steady-State Errors with Respect to Types of Inputs

- Any physical control system inherently suffers steady-state response to certain types of inputs.
- A system may have no steady-state error to a step input, but the same system exhibit nonzero steady-state error to a ramp input.
- Whether a given unity feedback system will exhibit steady-state error for a given type of input depends on the type of ***loop gain*** of the system.

Classification of Control System

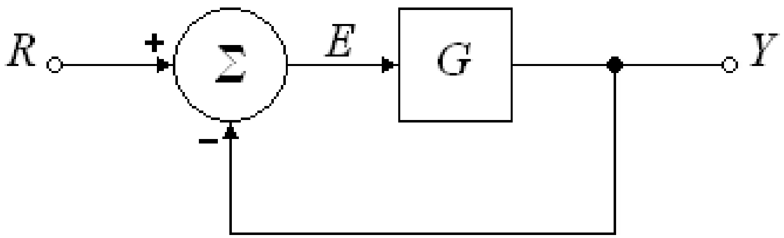
- Control systems may be ***classified according to their ability to track polynomial inputs***, or *in other words*, their ability to reach zero steady-state to step-inputs, ramp inputs, parabolic inputs and so on.

- This is a reasonable classification scheme because actual inputs may frequently be considered combinations of such inputs.

- The magnitude of the steady-state errors due to these individual inputs are indicative of the goodness of the system.

The Unity Feedback Control Case

Steady-State Error



$$\frac{Y(s)}{R(s)} = \frac{G(s)}{1+G(s)}$$

- Error: $e(t) = r(t) - y(t) \Rightarrow E(s) = R(s) - Y(s) = \dfrac{R(s)}{1+G(s)}$

- *Using the FVT, the **steady-state error** is given by*:

$$e_{ss} = \lim_{t\to\infty} e(t) = \lim_{s\to 0} sE(s) = \lim_{s\to 0} sR(s)\frac{1}{1+G(s)}$$

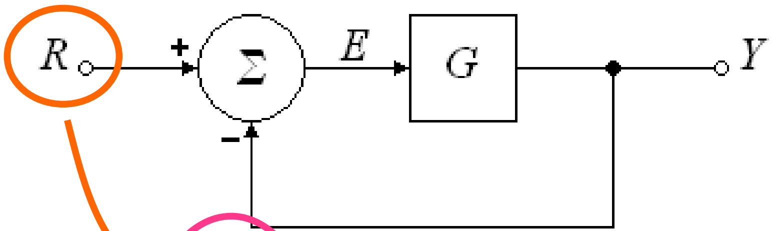
FVT

Steady-state error to polynomial input - Unity Feedback Control -

- Consider a ***polynomial input***:

$$r(t) = t^{k-1}u(t) \Rightarrow R(s) = \frac{1}{s^k}$$

- The ***steady-state error*** is then given by:



$$e_{ss} = \lim_{s\to 0} s\frac{1}{s^k}\frac{1}{1+G(s)} = \lim_{s\to 0} \frac{s}{s^k}\frac{1}{1+G(s)}$$

System Type

A *unity feedback system* is defined to be **type k** if

the feedback system guarantees:

$$e_{ss} = 0 \quad for \quad R(s) = \frac{1}{s^k}$$

$$|e_{ss}| < \infty \quad for \quad R(s) = \frac{1}{s^{k+1}}$$

System Type (cont'd)

- Since, for an input

$$R(s) = \frac{1}{s^k}$$

$$e_{ss} = \lim_{s\to 0} s \frac{1}{s^k} \frac{1}{1+G(s)} = \lim_{s\to 0} \frac{s}{s^k} \frac{1}{1+G(s)}$$

the *system* is called a **type k system** if:

$$\lim_{s\to 0} \frac{s}{s^k} \frac{1}{1+G(s)} = 0$$

$$\left| \lim_{s\to 0} \frac{s}{s^{k+1}} \frac{1}{1+G(s)} \right| < \infty$$

Example 1: Unity feedback

- Given a stable system whose the open-loop transfer function is:

$$G(s)=\frac{K(s-z_1)(s-z_2)\cdots}{s\,(s-p_1)(s-p_2)\cdots}=\frac{G_0(s)}{s}$$ subjected to inputs $$R(s)=\frac{1}{s^k}$$

$(p_i \neq 0)$

- Step function: $R(s)=1/s\,,\ k=1$

$$e_{ss}=\lim_{s\to 0}\frac{s}{s}\frac{1}{1+\frac{G_0(s)}{s}}=\lim_{s\to 0}\frac{s}{s}\frac{s}{s+G_0(s)}=\frac{0}{0+G_0(0)}=0$$

- Ramp function: $R(s)=1/s^2\,,\ k=2$

$$e_{ss}=\lim_{s\to 0}\frac{s}{s^2}\frac{1}{1+\frac{G_0(s)}{s}}=\lim_{s\to 0}\frac{s}{s^2}\frac{s}{s+G_0(s)}=\lim_{s\to 0}\frac{1}{s+G_0(s)}=\frac{1}{G_0(0)}\neq 0$$

→ The system is type 1

Example 2: Unity feedback

- Given a stable system whose the open-loop transfer function is:

$$G(s)=\frac{K(s-z_1)(s-z_2)\cdots}{s^2(s-p_1)(s-p_2)\cdots}=\frac{G_0(s)}{s^2}$$

subjected to inputs $(p_i \neq 0)$ $R(s)=\frac{1}{s^k}$

- Step function: $R(s)=1/s,\ k=1$

$$e_{ss}=\lim_{s\to 0}\frac{s}{s}\frac{1}{1+\frac{G_0(s)}{s^2}}=\lim_{s\to 0}\frac{s}{s}\frac{s^2}{s^2+G_0(s)}=\frac{0}{0+G_0(0)}=0$$

- Ramp function: $R(s)=1/s^2,\ k=2$

$$e_{ss}=\lim_{s\to 0}\frac{s}{s^2}\frac{1}{1+\frac{G_0(s)}{s^2}}=\lim_{s\to 0}\frac{s}{s^2}\frac{s^2}{s^2+G_0(s)}=\lim_{s\to 0}\frac{s}{s^2+G_0(s)}=\frac{0}{G_0(0)}=0$$

- Parabola function: $R(s)=1/s^3,\ k=3$

$$e_{ss}=\lim_{s\to 0}\frac{s}{s^3}\frac{1}{1+\frac{G_0(s)}{s^2}}=\lim_{s\to 0}\frac{s}{s^3}\frac{s^2}{s^2+G_0(s)}=\frac{1}{G_0(0)}\neq 0$$

$\rightarrow$ type 2

Example 3: Unity feedback

- Given a stable system whose the open loop transfer function is:

$$G(s) = \frac{K(s-z_1)(s-z_2)\cdots}{(s-p_1)(s-p_2)\cdots} = G_0(s)$$ subjected to inputs $(p_i \neq 0)$ $$R(s) = \frac{1}{s^k}$$

- Step function: $R(s) = 1/s,\ k=1$

$$e_{ss} = \lim_{s\to 0} \frac{s}{s}\frac{1}{1+G_0(s)} = \frac{1}{1+G_0(0)} \neq 0$$

$\rightarrow$ The system is type 0

- Impulse function: $R(s) = 1,\ k=0$

$$e_{ss} = \lim_{s\to 0} \frac{s}{1}\frac{1}{1+G_0(s)} = \frac{0}{G_0(0)} = 0$$

Summary – Unity Feedback

- Assuming $p_i \neq 0$ unity system loop transfers such as:

$$G(s) = \frac{K(s-z_1)(s-z_2)\cdots}{(s-p_1)(s-p_2)\cdots} = G_0(s) \quad \rightarrow \text{type 0}$$

$$G(s) = \frac{K(s-z_1)(s-z_2)\cdots}{s\,(s-p_1)(s-p_2)\cdots} = \frac{G_0(s)}{s} \quad \rightarrow \text{type 1}$$

$$G(s) = \frac{K(s-z_1)(s-z_2)\cdots}{s^2(s-p_1)(s-p_2)\cdots} = \frac{G_0(s)}{s^2} \quad \rightarrow \text{type 2}$$

$$G(s) = \frac{K(s-z_1)(s-z_2)\cdots}{s^n(s-p_1)(s-p_2)\cdots} = \frac{G_0(s)}{s^n} \quad \rightarrow \text{type n}$$

General Rule – Unity Feedback

- An unity feedback system is of ***type k*** if the open-loop transfer function of the system has:

k poles at s=0

In other words,

- An unity feedback system is of ***type k*** if the open-loop transfer function of the system has:

k integrators

Error Constants

- A *stable* ***unity*** *feedback system is* ***type k*** with respect to reference inputs if the **open loop transfer function has k poles at the origin**:

$$D(s)G(s)=\frac{(s-z_1)(s-z_2)\cdots}{s^k(s-p_1)(s-p_2)\cdots}=\frac{D_0(s)G_0(s)}{s^k}$$

Then the **error constant** is given by:

$$K_k=\lim_{s\to 0}s^k D(s)G(s)=D_0(0)G_0(0)$$

- The higher the constants, the smaller the steady-state error.

Error Constants

- For a ***Type 0 System***, the error constant, called ***position constant***, is given by:

$$K_p = \lim_{s \to 0} D(s)G(s) \qquad \text{(dimensionless)}$$

- For a ***Type 1 System***, the error constant, called ***velocity constant***, is given by:

$$K_v = \lim_{s \to 0} sD(s)G(s) \qquad (\sec^{-1})$$

- For a ***Type 2 System***, the error constant, called ***acceleration constant,*** is given by:

$$K_a = \lim_{s \to 0} s^2 D(s)G(s) \qquad (\sec^{-2})$$

Example:

- A temperature control system is found to have zero error to a constant tracking input and an error of 0.5°C to a tracking input that is linear in time, rising at the rate of 40°C/sec.
- What is the system type?

The system is type 1

- What is the steady-state error?

$$e_{ss} = 0.5^o C = \frac{40^o C / sec}{K_v}$$

- What is the error constant?

$$K_v = \frac{40^o C / sec}{0.5^o C} = 80\ sec^{-1}$$

Conclusion

- *Classifying a system as* ***k type*** indicates the ability of the system to **achieve zero steady-state error to polynomials r(t) of degree less but not equal to k.**

- The system is ***type k*** if the **error is zero to all polynomials r(t) of degree less than k but non-zero for a polynomial of degree k**.

Conclusion

- A *stable* ***unity*** *feedback system is* ***type k*** with respect to reference inputs if the **loop transfer function has k poles at the origin**:

$$D(s)G(s) = \frac{(s-z_1)(s-z_2)\cdots}{s^k(s-p_1)(s-p_2)\cdots}$$

$$K_k = \lim_{s \to 0} s^k D(s)G(s)$$

- Then the **error constant** is given by:

Steady-State Errors as a function of System Type – Unity Feedback

System type	Step input	Ramp input	Parabola input
Type 0	$\frac{1}{1+K_p}$	∞	∞
Type 1	0	$\frac{1}{K_v}$	∞
Type 2	0	0	$\frac{1}{K_a}$

The Classical Three- Term Controllers

Basic Operations of a Feedback Control

Think of what goes on in domestic hot water thermostat:

- The temperature of the water is measured.
- Comparison of the measured and the required values provides an error, *e.g. "too hot' or 'too cold'.*
- On the basis of error, a control algorithm decides what to do.

  $\rightarrow$ *Such an algorithm might be:*
  - *If the temperature is too high then turn the heater off.*
  - *If it is too low then turn the heater on*
- The adjustment chosen by the control algorithm is applied to some adjustable variable, *such as the power input to the water heater.*

Feedback Control Properties

- ***A feedback control system seeks to bring the measured quantity to its required value or set-point.***
- The control system *does not need to know why the measured value is not currently what is required*, only that is so.
- There are two *possible causes of such a disparity*:
  - The system has been disturbed.
  - The setpoint has changed. In the absence of external disturbance, a change in setpoint will introduce an error. The control system will act until the measured quantity reach its new setpoint.

The PID Algorithm

- The **PID algorithm** is the *most popular feedback controller algorithm used*. It is a robust easily understood algorithm that can provide *excellent control performance* despite the varied dynamic characteristics of processes.

- As the name suggests, the PID **algorithm** consists of ***three basic modes***:

the ***Proportional*** mode,

the ***Integral*** mode

& the ***Derivative*** mode.

P, PI or PID Controller

- When utilizing the PID algorithm, it is necessary to decide which modes are to be used (P, I or D) and then ***specify the parameters (or settings) for each mode used***.

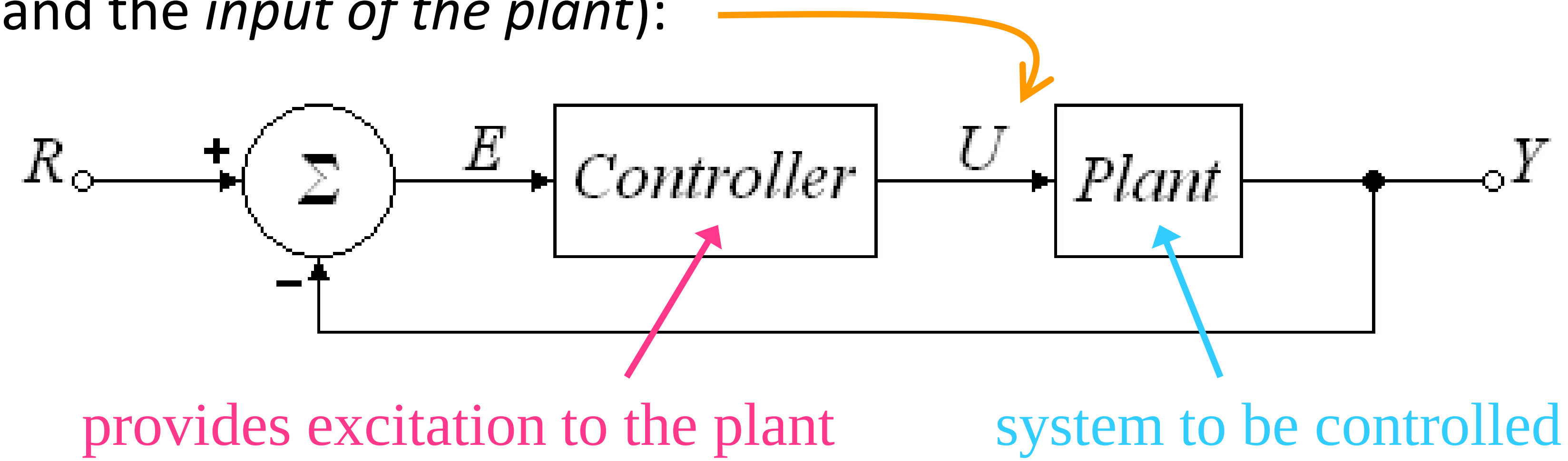
- Generally, three basic algorithms are used: ***P, PI or PID***.

- Controllers are designed to eliminate the need for continuous operator attention.

  → *Cruise control in a car and a house thermostat* are common examples of *how controllers are used to automatically adjust some variable to hold a measurement (or* ***process variable****) to a desired variable (or* ***set-point****)*

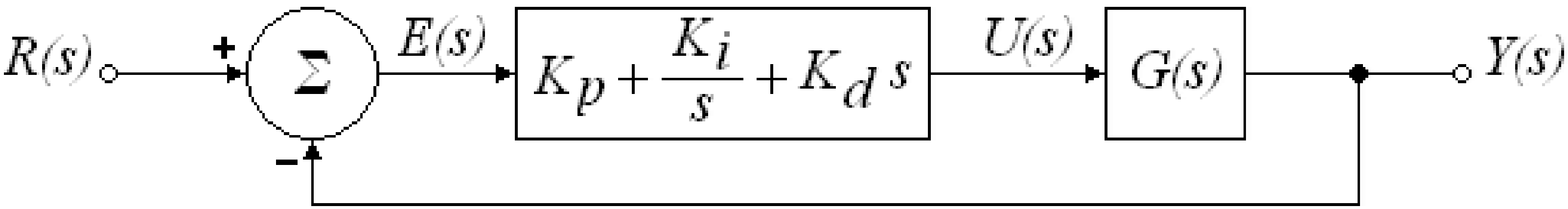
Controller Output

- The *variable being controlled* is the ***output of the controller*** (and the *input of the plant*):



- The output of the controller will change in response to a change in measurement or set-point (that said a change in the tracking error)

PID Controller



- In the *s*-domain, the PID controller may be represented as:

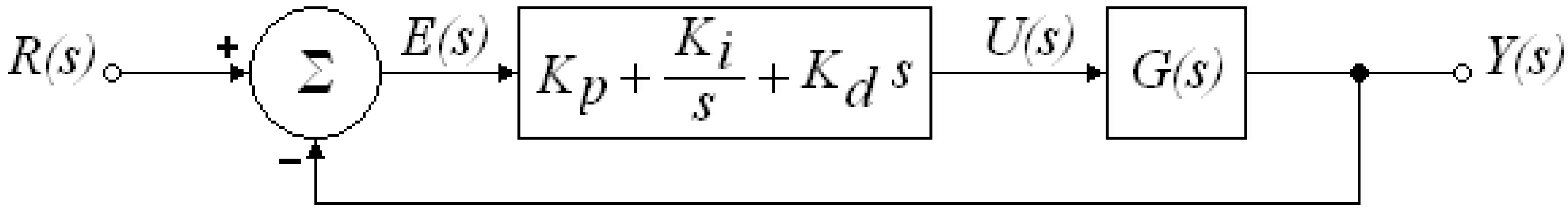
$$U(s) = \left(K_p + \frac{K_i}{s} + K_d s \right) E(s)$$

- In the time domain:

$$u(t) = K_p e(t) + K_i \int_0^t e(t)dt + K_d \frac{de(t)}{dt}$$

proportional gain integral gain derivative gain

PID Controller



- In the time domain:

$$u(t) = K_p e(t) + K_i \int_0^t e(t)dt + K_d \frac{de(t)}{dt}$$

- The signal *u(t)* will be sent to the plant, and a new output *y(t)* will be obtained. This new output *y(t)* will be sent back to the sensor again to find the new error signal *e(t).* The controllers takes this new error signal and computes its derivative and its integral gain. This process goes on and on.

Definitions

- In the time domain:

$$u(t) = K_p e(t) + K_i \int_0^t e(t)dt + K_d \frac{de(t)}{dt}$$

$$= K_p \left(e(t) + \frac{1}{T_i} \int_0^t e(t)dt + T_d \frac{de(t)}{dt} \right)$$

integral time constant — derivative time constant

$$\text{where} \quad T_i = \frac{K_p}{K_i}, \qquad T_d = \frac{K_d}{K_i}$$

derivative gain

proportional gain — integral gain

Controller Effects

- A **proportional controller** (P) ***reduces error responses to disturbances***, but *still allows a steady-state error.*

- When the controller includes a term proportional to the integral of the error (I), then the ***steady state error to a constant input is eliminated***, although typically *at the cost of deterioration in the dynamic response.*

- A **derivative control** (D) typically ***makes the system better damped and more stable.***

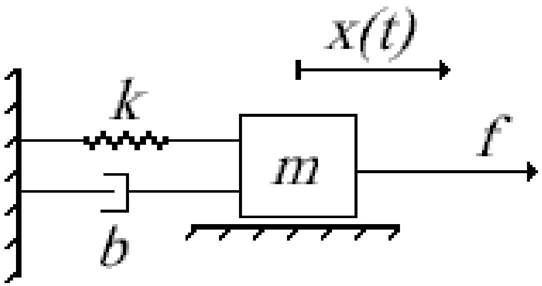
Closed-loop Response

	Rise time	Maximum overshoot	Settling time	Steady-state error
P	**Decrease**	Increase	Small change	**Decrease**
I	**Decrease**	Increase	Increase	**Eliminate**
D	Small change	**Decrease**	**Decrease**	Small change

- Note that these correlations may not be exactly accurate, because P, I and D gains are dependent of each other.

Example problem of PID

- Suppose we have a simple mass, spring, damper problem.



- The dynamic model is such as: $$m\ddot{x} + b\dot{x} + kx = f$$

- Taking the Laplace Transform, we obtain:

$$ms^2 X(s) + bsX(s) + kX(s) = F(s)$$

- The Transfer function is then given by:

$$\frac{X(s)}{F(s)} = \frac{1}{ms^2 + bs + k}$$

Example problem (cont'd)

- Let

$$m = 1kg,\ b = 10N.s/m,\ k = 20N/m,\ \ f = 1N$$

- By plugging these values in the transfer function:

$$\frac{X(s)}{F(s)} = \frac{1}{s^2 + 10s + 20}$$

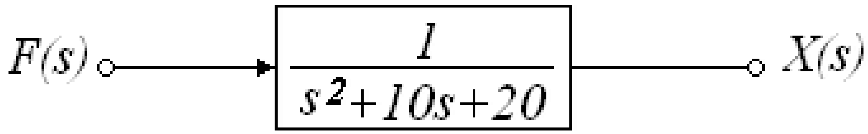
- The goal of this problem is to show you how each of $K_p, K_i\ and\ K_d$ contribute to obtain:

fast rise time,

minimum overshoot,

no steady-state error.

Ex (cont'd): No controller



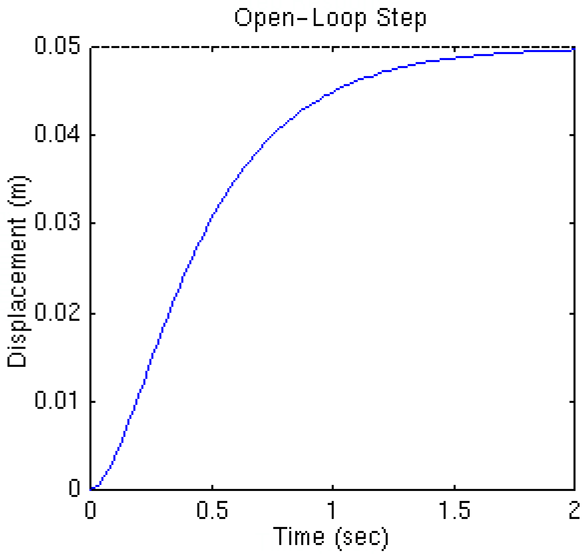
- The (***open***) loop transfer function is given by:

$$\frac{X(s)}{F(s)} = \frac{1}{s^2 + 10s + 20}$$

- The steady-state value for the output in case of STEP input is:

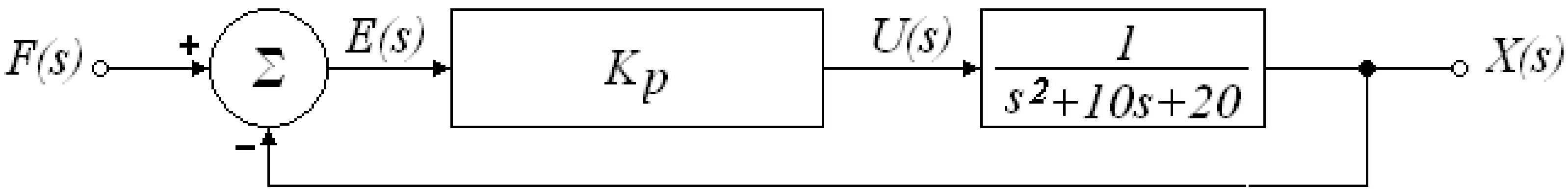
$$x_{ss} = \lim_{t \to \infty} x(t) = \lim_{s \to 0} sX(s) = \lim_{s \to 0} sF(s)\frac{X(s)}{F(s)} = \frac{1}{20}$$

Ex (cont'd): Open-loop step response



- 1/20=0.05 is the *final value* of the output to an *unit* step input.
- This corresponds to a **steady-state error of 95%, *quite large!***
- The ***settling time is about 1.5 sec.***

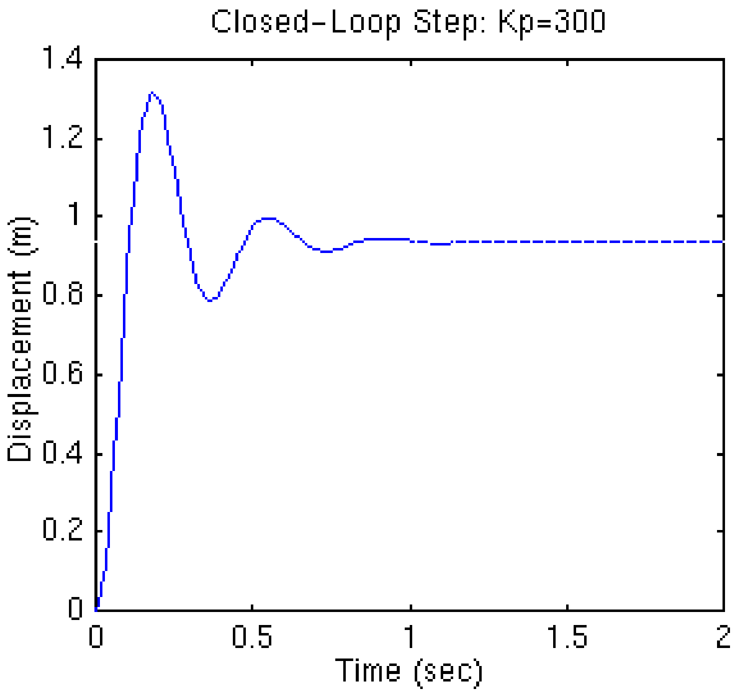
Ex (cont'd): Proportional Controller



- The closed loop transfer function is given by:

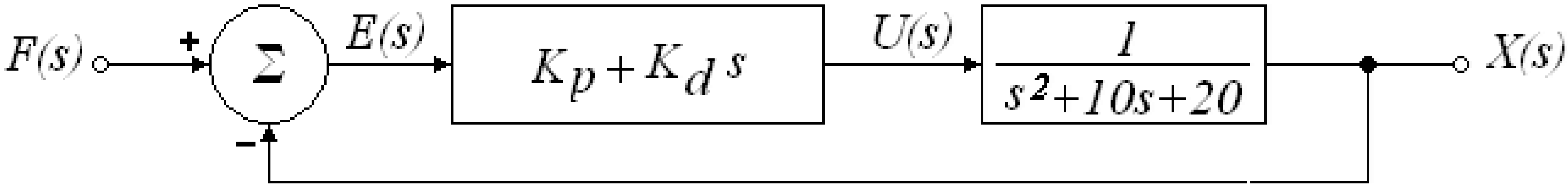
$$\frac{X(s)}{F(s)} = \frac{\dfrac{K_p}{s^2+10s+20}}{1+\dfrac{K_p}{s^2+10s+20}} = \frac{K_p}{s^2+10s+(20+K_p)}$$

Ex (cont'd): Proportional control



- Let $K_p = 300$
- The above plot shows that the ***proportional controller reduced both the rise time and the steady-state error***, *increased the overshoot*, and *decreased the settling time by small amount.*

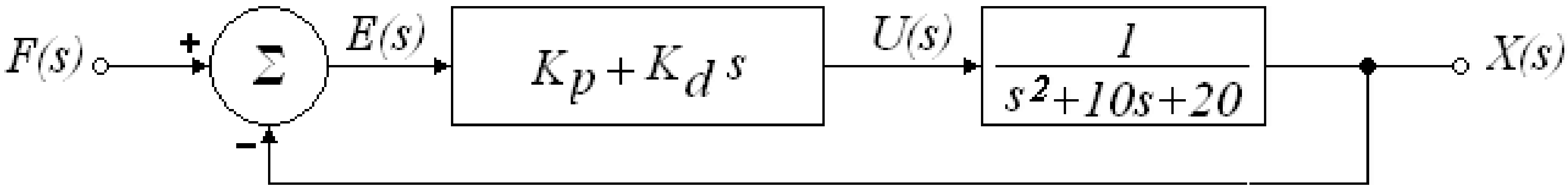
Teamwork Ex on PD Controller



- Find the closed loop transfer function if:

$$K_p = 300, \quad K_d = 10$$

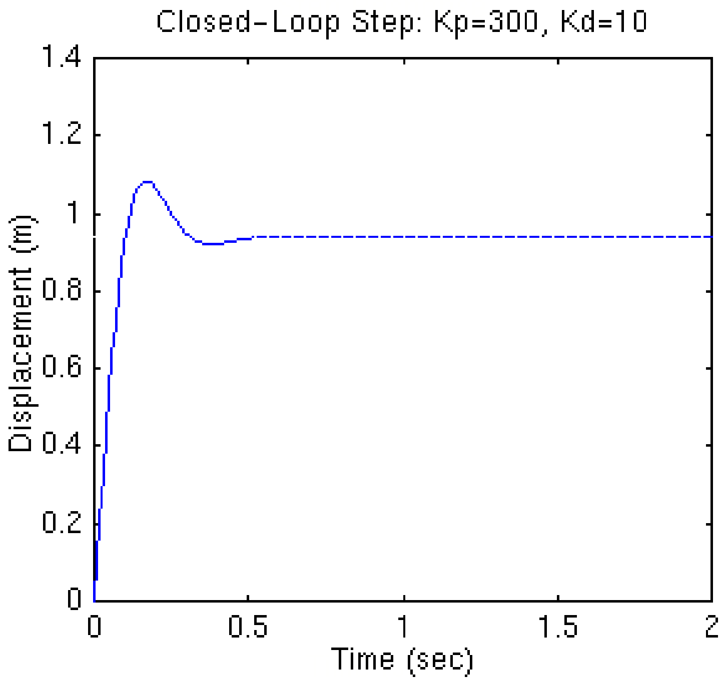
Ex (cont'd): PD Controller



- The closed loop transfer function is given by:

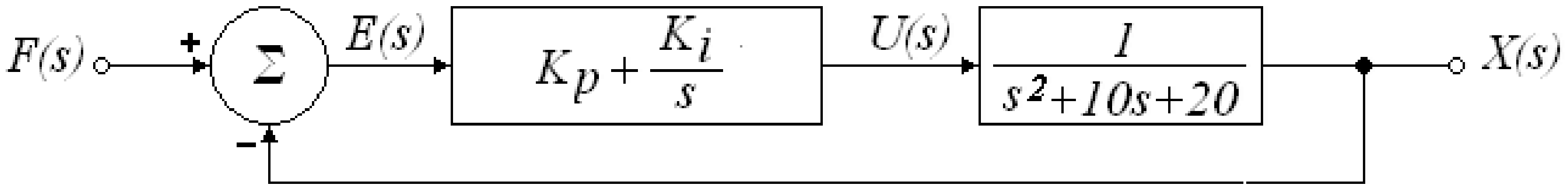
$$\frac{X(s)}{F(s)} = \frac{\dfrac{K_p + K_d s}{s^2 + 10s + 20}}{1 + \dfrac{K_p + K_d s}{s^2 + 10s + 20}} = \frac{K_p + K_d s}{s^2 + (10 + K_d)s + (20 + K_p)}$$

Ex (cont'd): PD control



- Let $K_p = 300, \; K_d = 10$
- This plot shows that the ***proportional derivative controller reduced both the overshoot and the settling time***, and *had small effect on the rise time and the steady-state error*.

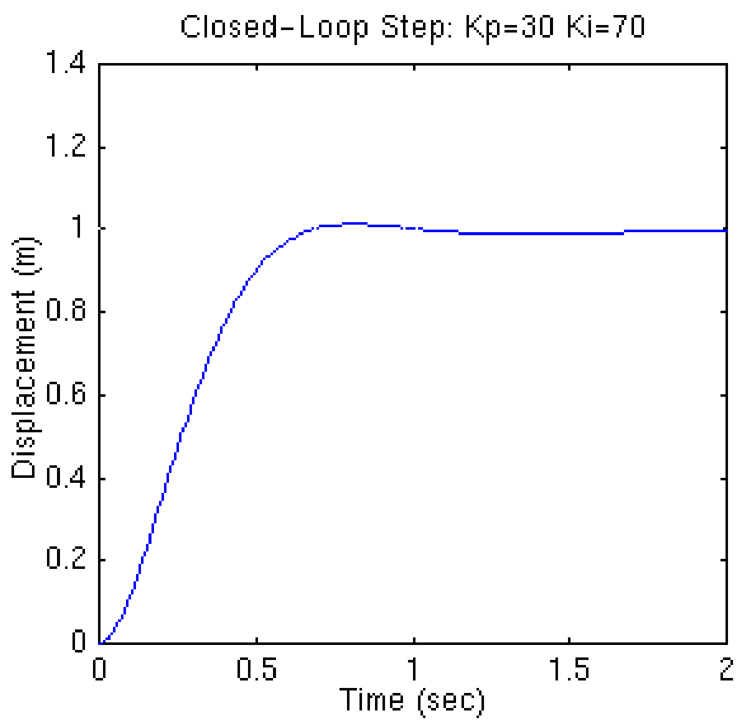
Ex (cont'd): PI Controller



- The closed loop transfer function is given by:

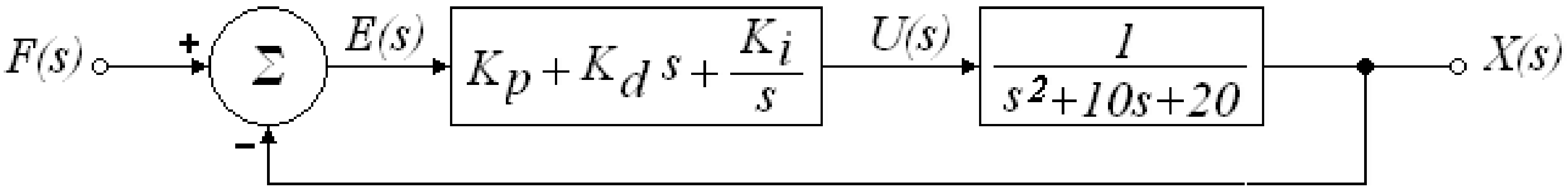
$$\frac{X(s)}{F(s)} = \frac{\dfrac{K_p + K_i/s}{s^2 + 10s + 20}}{1 + \dfrac{K_p + K_i/s}{s^2 + 10s + 20}} = \frac{K_p s + K_i}{s^3 + 10s^2 + (20 + K_p)s + K_i}$$

Ex (cont'd): PI Controller



- Let $K_p = 30, \; K_i = 70$
- We have reduced the proportional gain because the integral controller also ***reduces the rise time and increases the overshoot*** as the proportional controller does (double effect).
- The above response shows that the ***integral controller eliminated the steady-state error***.

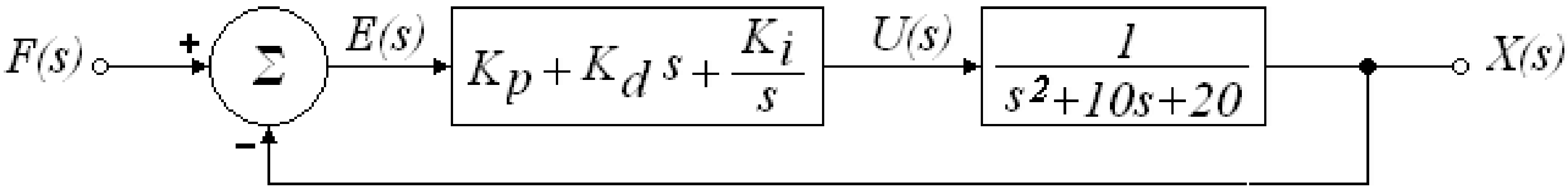
Teamwork Ex on PID Controller



- Find the closed loop transfer function if:

$$K_p = 350, \; K_i = 300, \; K_d = 5500$$

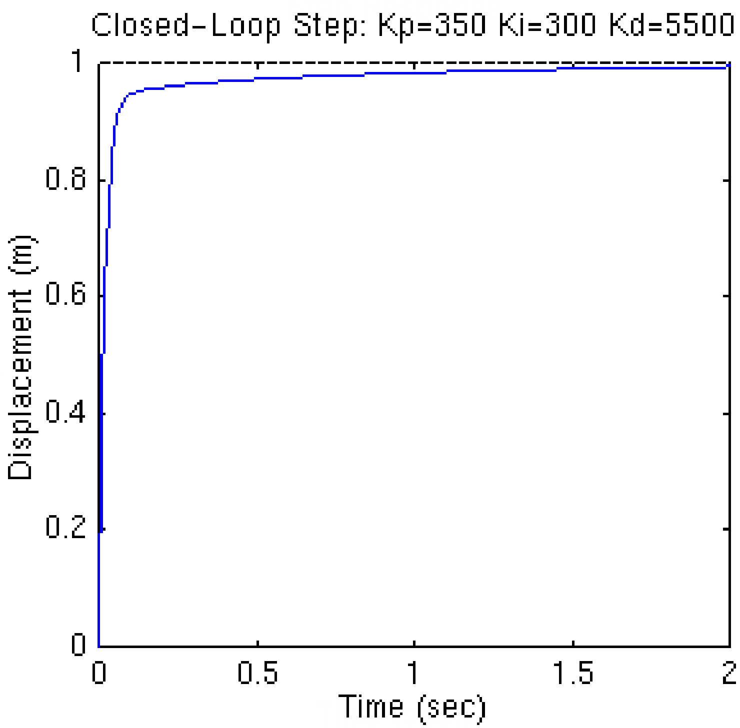
Ex (cont'd): PID Controller



- The closed loop transfer function is given by:

$$\frac{X(s)}{F(s)} = \frac{\dfrac{K_p + K_d s + K_i / s}{s^2 + 10s + 20}}{1 + \dfrac{K_p + K_d s + K_i / s}{s^2 + 10s + 20}} = \frac{K_d s^2 + K_p s + K_i}{s^3 + (10 + K_d) s^2 + (20 + K_p) s + K_i}$$

Ex (cont'd): PID Controller

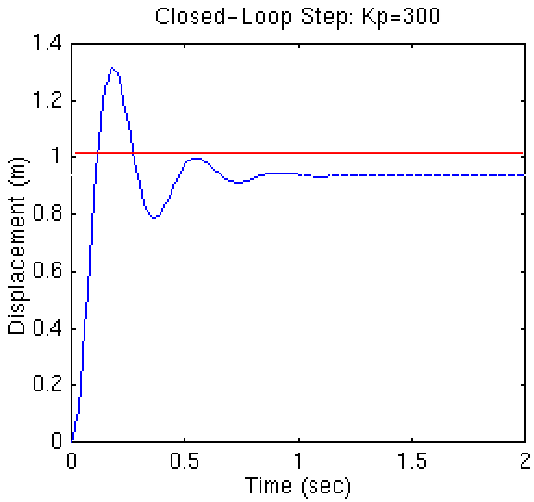


- Let $K_p = 350,\ K_i = 300,$ $K_d = 5500$

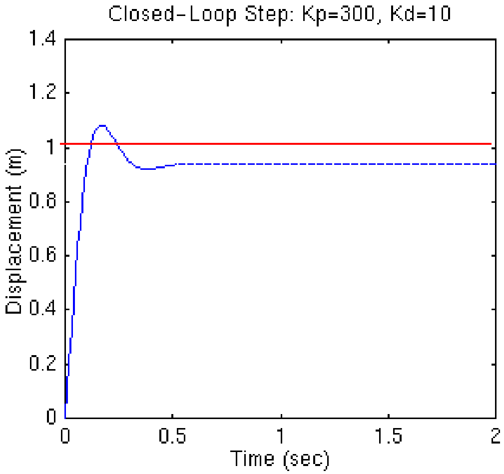
- Now, we have obtained the system with **no overshoot, fast rise time, and no steady-state error.**

Ex (cont'd): Summary

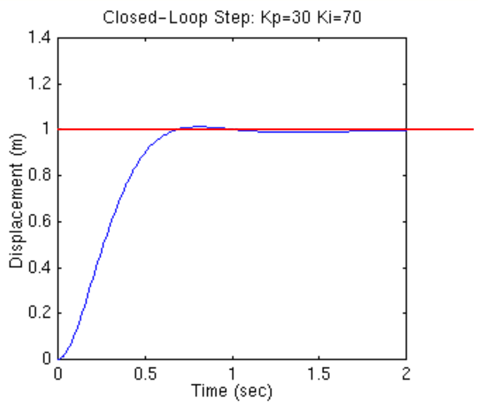
P



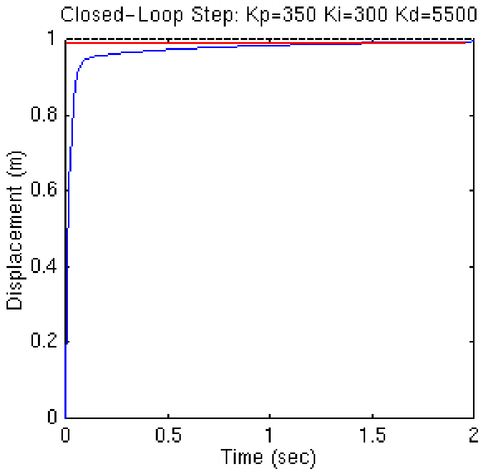
PD



PI



PID



PID Controller Functions

- Output feedback

  $\rightarrow$ from ***Proportional action***

  compare output with set-point

- Eliminate steady-state offset (=error)

  $\rightarrow$ from ***Integral action***

  apply constant control even when error is zero

- Anticipation

  $\rightarrow$ From ***Derivative action***

  react to rapid rate of change before errors grows too big

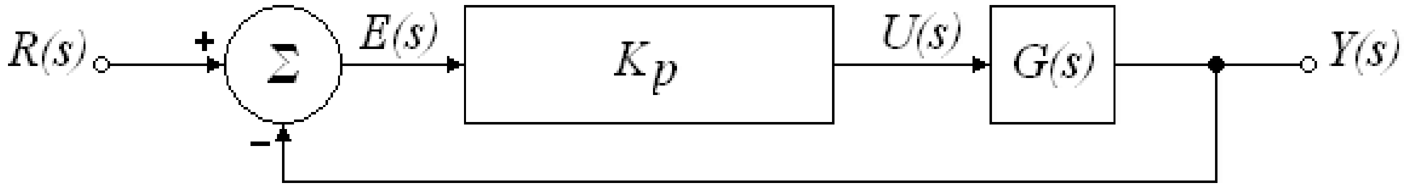
Effect of Proportional, Integral & Derivative Gains on the Dynamic Response

Proportional Controller

- Pure gain (or ***attenuation***) since:

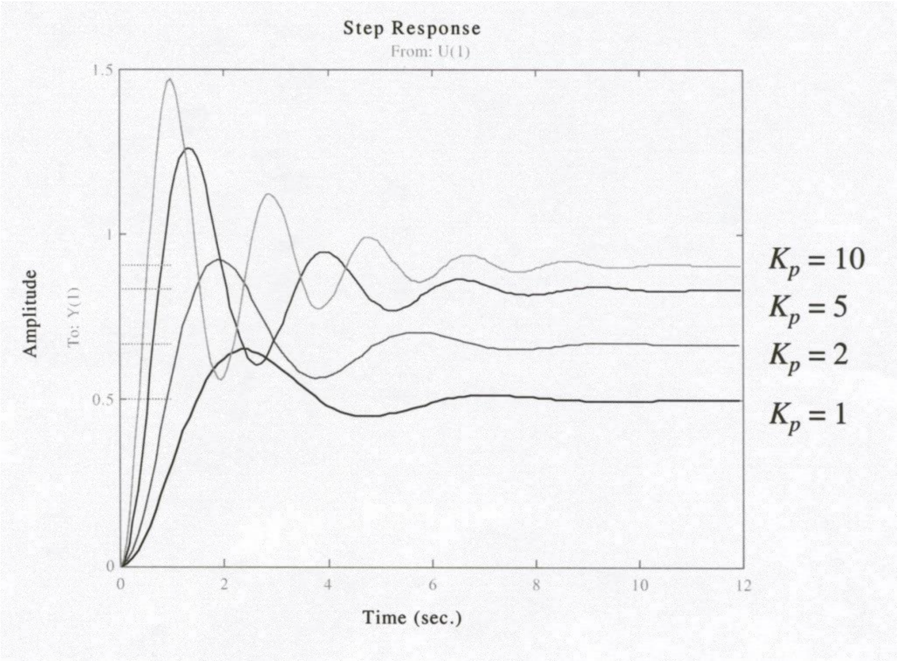
  the controller input is error

  the controller output is a proportional gain



$$E(s)K_p = U(s) \Rightarrow u(t) = K_p e(t)$$

Change in gain in P controller



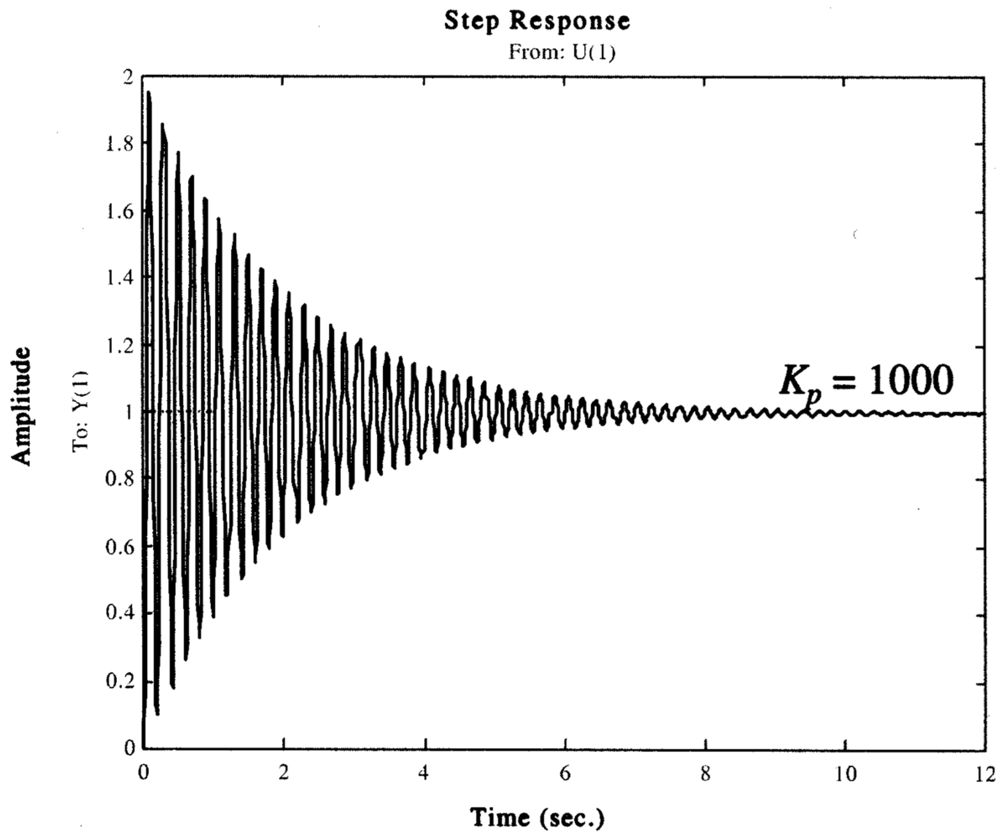
- **Increase in gain**:

  $\rightarrow$ Upgrade both steady-state and transient responses

  $\rightarrow$ Reduce steady-state error

  $\rightarrow$ ***Reduce stability!***

P Controller with *high* gain



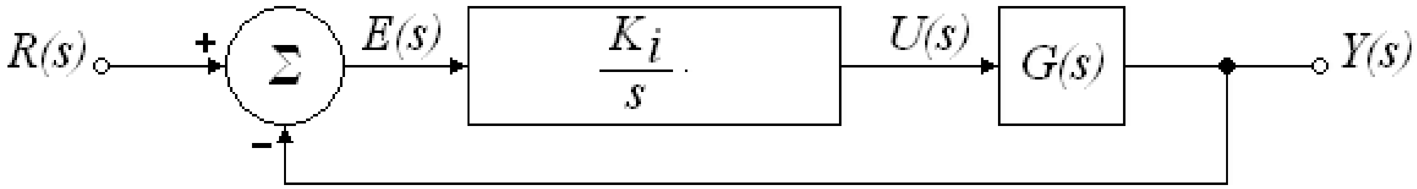
Integral Controller

- Integral of error with a constant gain

$\rightarrow$ increase the system type by 1

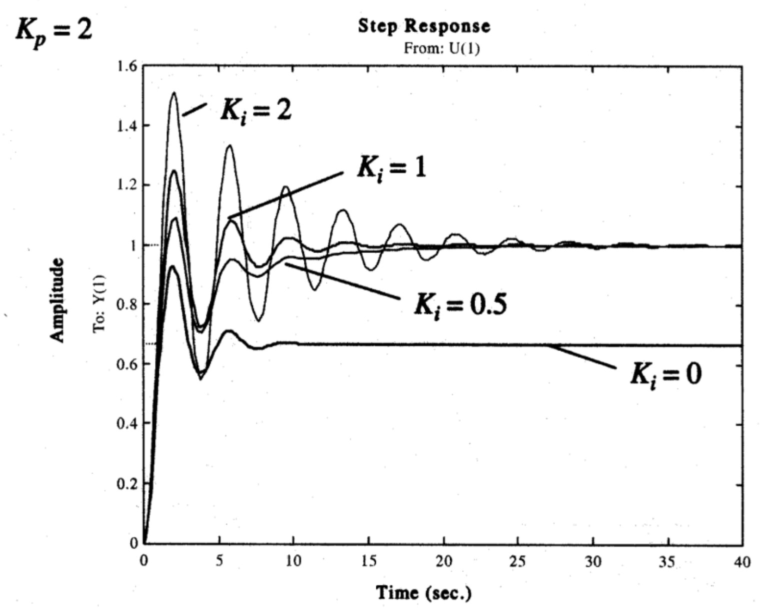
$\rightarrow$ *eliminate steady-state error for a unit step input*

$\rightarrow$ amplify overshoot and oscillations



$$E(s)\frac{K_i}{s} = U(s) \Rightarrow u(t) = K_i \int_0^t e(t)dt$$

Change in gain for PI controller



- **Increase in gain**:
  - → Do not upgrade steady-state responses
  - → Increase slightly settling time
  - → ***Increase oscillations and overshoot!***

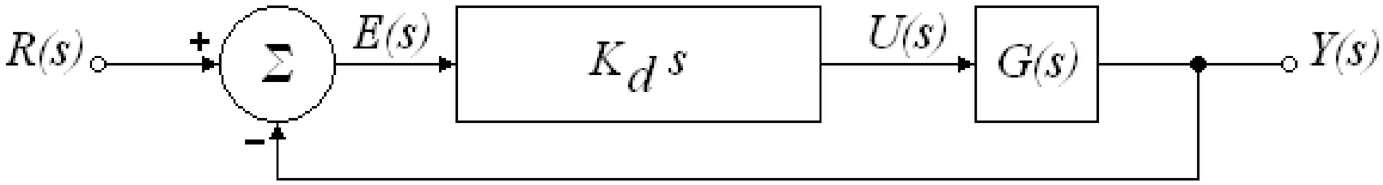
Derivative Controller

- Differentiation of error with a constant gain

$\rightarrow$ detect rapid change in output

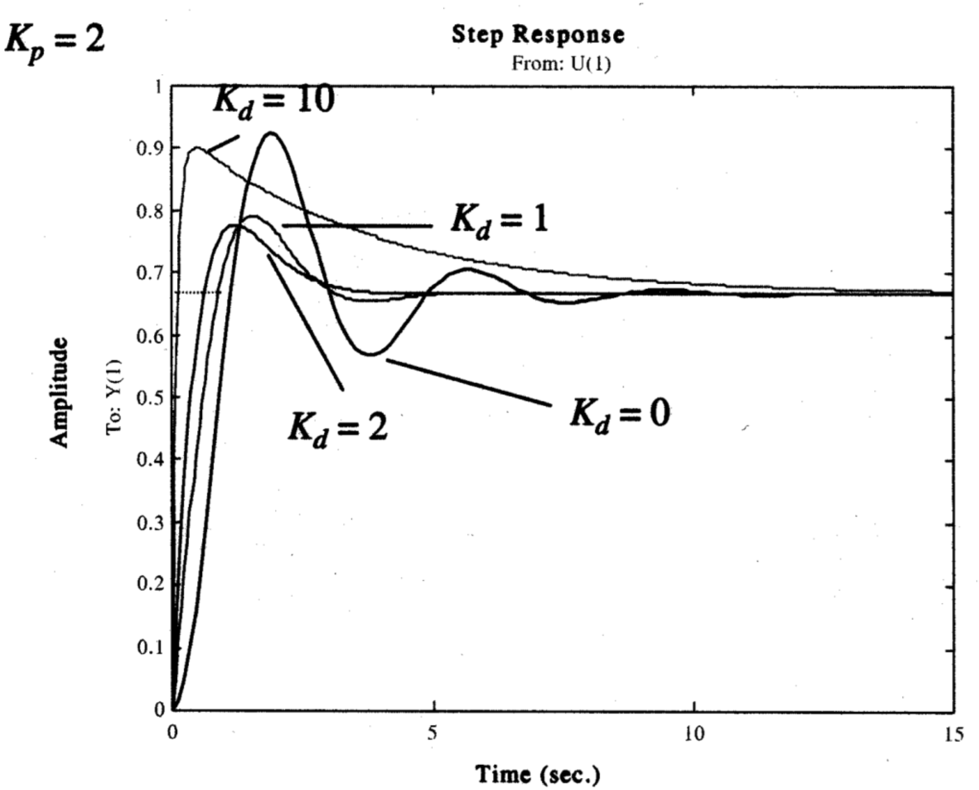
$\rightarrow$ *reduce overshoot and oscillation*

$\rightarrow$ do not affect the steady-state response



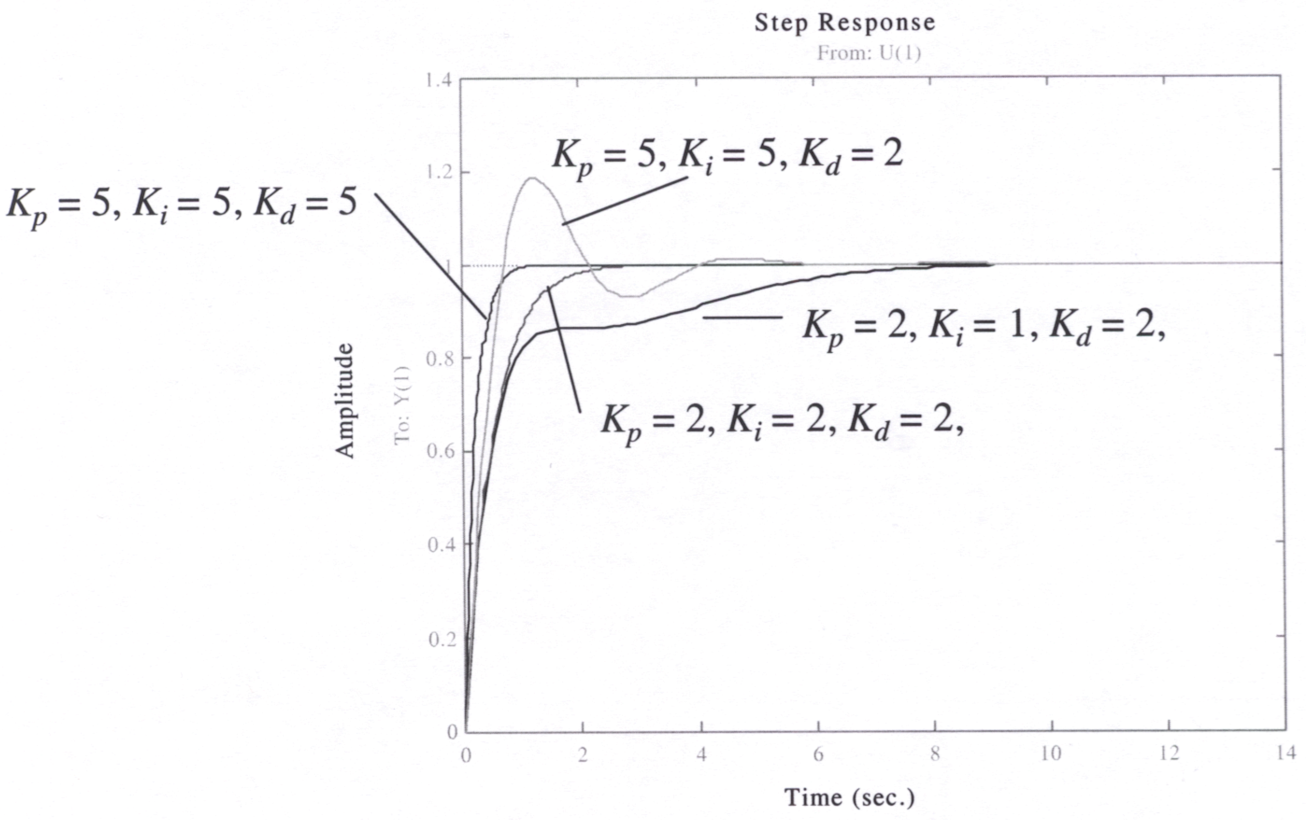
$$E(s)K_d s = U(s) \Rightarrow u(t) = K_d \frac{de(t)}{dt}$$

Effect of change for gain PD controller



- **Increase in gain**:
  - → Upgrade transient response
  - → Decrease the peak and rise time
  - → ***Increase overshoot and settling time!***

Changes in gains for PID Controller



Conclusions

- **Increasing the proportional feedback gain** ***reduces steady-state errors***, but high gains almost always ***destabilize the system.***
- **Integral control** provides ***robust reduction in steady-state errors***, but often ***makes the system less stable.***
- **Derivative control** usually ***increases damping and improves stability,*** but has almost ***no effect on the steady state error***
- These ***3 kinds of control combined*** from the **classical PID controller**

Conclusion - PID

- The standard PID controller is described by the equation:

$$U(s)=\left(K_p+\frac{K_i}{s}+K_d s\right)E(s)$$

$$or \quad U(s)=K_p\left(1+\frac{1}{T_i}s+T_d s\right)E(s)$$

Application of PID Control

- PID regulators provide reasonable control of most industrial processes, provided that the performance demands is not too high.
- PI control are generally adequate when plant/process dynamics are essentially of 1^{st}-order.
- PID control are generally ok if dominant plant dynamics are of 2^{nd}-order.
- More elaborate control strategies needed if process has long time delays, or lightly-damped vibrational modes